

# Comparison between Commensurate and Non-commensurate Fractional Systems

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**Abstract**—This article deals with fractional systems that represent better physical process and guarantee a very small number of parameters that can reduce the computation time. It focuses in particular on the state-space representation which highlights the state variables and allows to study the internal behavior of the system taking into account the initial state. Moreover, this representation adapts better to the multiple input multiple-output case. It also discusses the discretization of fractional system to finally adapt the Model Predictive Control to apply it and shows its efficiency and performance in these systems. The main objective of this article is to compare the commensurate and non-commensurate fractional models performance, calculation time and ease of use.

**Keywords**—discretization; state-space; fractional; calculation time

## I. INTRODUCTION

Over the last few years, many theoretical and practical contributions showed the importance of fractional systems and their interest in different applications of modeling, identification and control of physical systems. Several control strategies have been developed and adapted for fractional systems such as the PID controller, sliding mode control and predictive control. In different disciplines such as electricity, chemistry, biology, economics, automation and signal processing. Some researchers have compared the fractional models with the classical integer models. The results have shown that fractional model represents systems with much lower number of parameters than those of integer model.

The most studied physical phenomena and most used during modeling or identification are mentioned in [1].

One of these phenomena is the attenuation of the movement of water on dikes, especially those with cavities or depressions trapping air pockets that can be compressed by water.

There is also the viscoelasticity of the materials having mechanical properties strongly dependent on the frequency over many decades of frequency, where the number of parameters is very large. As a result, calculations on the model take time and produce high order differential equations. Which is solved by using a fractional model with a number of parameters very reduced in [2].

Ref [3] treated another phenomenon that requires the use of the fractional model which is the Randles model that is frequently used in the literature for modeling lead-acid batteries. This model results from a simplified solution of the electrochemical diffusion equation in the batteries (Fick's law).

To finish, the diffusion of heat in a semi-infinite environment subjected to a heat flux  $q(t)$  on its surface boundary  $S$ . In [4, 5], authors demonstrate that the mathematical equations describing the unidirectional heat transfer in the environment reveal a real order of derivation of the temperature at the point of abscissa  $x = 0$ .

Almost all articles dealing with fractional systems focus on commensurate order systems and the developed controls are based on the transfer function model. But in practice the identification programs give better results in free identification. Therefore the orders of systems can be arbitrary, this type is named non-commensurate order. This can impose problem because in the case of non-commensurate the use of the classic tools becomes impossible, moreover the programming becomes more complicated.

This paper compares the commensurate and non-commensurate fractional system discussing the advantages and the disadvantages of each model. The models used in this paper are in the form of a state-space representations that make it easier to study the internal behavior of systems and adapt better to MIMO systems.

The first section of this article quotes the different representations of fractional systems as well as the transition between them. A second section explores the method used to pass from a continuous model to a discrete model. Section 3 will present the predictive control that will be applied on the fractional model. In Section 5 we have implemented different methods to compare commensurate and non-commensurate fractional systems.

## II. GENERAL FRACTIONAL SYSTEM REPRESENTATION

A generalized fractional system can be represented by the following equation [6, 7]:

$$y(t) + \sum_{i=1}^n a_i D^{\alpha_i} y(t) = \sum_{i=1}^m b_i D^{\beta_i} u(t) \quad (1)$$

As the system is relaxed  $y(t) = u(t) = 0$  for  $t \leq 0$ , the Laplace transform of  $D^{\alpha_i} y(t)$  and  $D^{\beta_i} u(t)$  are respectively  $s^{\alpha_i} Y(s)$  and  $s^{\beta_i} U(s)$ , where  $Y(s)$  and  $U(s)$  are the Laplace transforms of  $y(t)$  and  $u(t)$ . Applying the Laplace transformation to (1) we obtain:

$$Y(s) + \sum_{i=1}^n a_i s^{\alpha_i} Y(s) = \sum_{i=1}^m b_i s^{\beta_i} U(s) \quad (2)$$

The transfer function can be deduced from the previous equation:

$$G(s) = \frac{Y(s)}{U(s)} = \frac{\sum_{i=1}^m b_i s^{\beta_i}}{1 + \sum_{i=1}^n a_i s^{\alpha_i}} \quad (3)$$

The generalized state space model corresponding to the multivariable transfer function is:

$$\begin{cases} D^{(\alpha)}(x) &= Ax + Bu \\ y &= Cx + Du \end{cases} \quad (4)$$

Where:

$$D^{(\alpha)}(x) = \left[ \frac{d^{\alpha_1}}{dt^{\alpha_1}} x_1, \frac{d^{\alpha_2}}{dt^{\alpha_2}} x_2 \cdots \frac{d^{\alpha_n}}{dt^{\alpha_n}} x_n \right]^T \quad (5)$$

The passage from the state-space representation to the transfer-function representation can be deduced as in the integer case by taking the Laplace transform and considering the zero initial conditions [8], it is given by:

$$G(s) = C \left[ (s^{(\alpha)} I_n - A)^{-1} \right] B + D \quad (6)$$

On the other hand, to go from the transfer function to the state representation there is a difference. This difference is due to the presence of fractional derivation orders that must be taken into account during transformation. As mentioned, the transfer function of fractional systems is represented as follows:

$$G(s) = \frac{b_m s^{\beta_m} + b_{m-1} s^{\beta_{m-1}} + \cdots + b_1 s^{\beta_1} + b_0}{s^{\alpha_n} + a_1 s^{\alpha_{n-1}} + \cdots + a_{n-1} s^{\alpha_1} + a_n} \quad (7)$$

With

$$\alpha_n > \alpha_{n-1} > \cdots > \alpha_2 > \alpha_1$$

and

$$\beta_m > \beta_{m-1} > \cdots > \beta_2 > \beta_1$$

Let  $\tilde{\alpha}$  be the vector obtained from the concatenation of the fractional numbers  $\alpha_i$  and  $\beta_i$  such that:

$$\tilde{\alpha} = [\tilde{\alpha}_{n+m} \tilde{\alpha}_{n+m-1} \tilde{\alpha}_{n+m-2} \cdots \tilde{\alpha}_2 \tilde{\alpha}_1] \quad (8)$$

With

$$\tilde{\alpha}_{n+m} > \tilde{\alpha}_{n+m-1} > \tilde{\alpha}_{n+m-2} > \cdots > \tilde{\alpha}_2 > \tilde{\alpha}_1$$

Let consider the continuous state-space model given by:

$$\begin{cases} D^\gamma(x) &= A_c x + B_c u \\ y &= C_c x \end{cases} \quad (9)$$

with

$$A_c = \begin{pmatrix} 0 & 1 & \cdots & 0 & 0 \\ 0 & 0 & & 0 & 0 \\ \vdots & & \ddots & & \vdots \\ 0 & 0 & & 0 & 1 \\ \tilde{a}_{n+m} & \tilde{a}_{n+m-1} & \cdots & \tilde{a}_2 & \tilde{a}_1 \end{pmatrix}, \quad B_c = \begin{pmatrix} 0 \\ \vdots \\ 0 \\ 1 \end{pmatrix}$$

$$C_c = (\tilde{c}_1 \quad \tilde{c}_2 \quad \cdots \quad \tilde{c}_{n+m-1} \quad \tilde{c}_{n+m})$$

and

$$D^\gamma x = [D^{\tilde{\alpha}_1} x_1 \quad \cdots \quad D^{(\tilde{\alpha}_{n+m} - \tilde{\alpha}_{n+m-1})} x_{n+m}] \quad (10)$$

Where the corresponding transfer function model  $H(s)$  is given by:

$$H(s) = \frac{\tilde{c}_1 + \tilde{c}_2 s^{\tilde{\alpha}_1} + \tilde{c}_3 s^{\tilde{\alpha}_1 + \tilde{\alpha}_2} + \cdots}{s^{\tilde{\alpha}_1 + \tilde{\alpha}_2 + \cdots + \tilde{\alpha}_{n+m}} + \cdots} \quad (11)$$

$$\frac{\cdots + \tilde{c}_{n+m} s^{\tilde{\alpha}_1 + \tilde{\alpha}_2 + \cdots + \tilde{\alpha}_{n+m-1}}}{\cdots + \tilde{a}_{n+m-2} s^{\tilde{\alpha}_1 + \tilde{\alpha}_2} + \tilde{a}_{n+m-1} s^{\tilde{\alpha}_1} \tilde{a}_{n+m}}$$

Since  $H(s)$  numerator and denominator contain  $(n + m)$  terms, it is then sufficient to sort them in order to isolate  $m$  terms for which the fractional orders correspond to those of  $G(s)$  numerator and  $n$  terms for which the fractional orders correspond to those of  $G(s)$  denominator. The procedure of selection of the terms  $\tilde{c}_i$  and  $\tilde{a}_i$  is summarized in (12).

$$\begin{cases} \tilde{a}_{n+m} = a_n & \tilde{c}_1 = b_0 \\ \text{if } \tilde{\alpha}_i = \beta_j & \text{then } \tilde{c}_{i+1} = b_j \text{ and } \tilde{a}_{n+m-i} = 0 \\ \text{if } \tilde{\alpha}_i = \alpha_j & \text{then } \tilde{c}_{i+1} = 0 \text{ and } \tilde{a}_{n+m-i} = a_{n-j} \end{cases} \quad (12)$$

$$i = 1, \dots, n + m - 1 \quad \text{and} \quad j = 1, \dots, n + m - 1$$

In this case of generalized fractional systems, the number of state variables is equal to the sum of dimensions of the numerator and denominator polynomials of the transfer function  $(n + m)$ .

### III. DISCRETIZATION OF FRACTIONAL STATE-SPACE MODEL

Contrary to the commensurate case, discretization in the case of non-commensurate fractional systems must take into account the plurality of derivations of state variables.

To move from a continuous model to a discrete model it is necessary to use this approximation [9, 10, 11]:

$$D^\gamma x(t) = \frac{1}{T_s^\gamma} \sum_{j=0}^p (-1)^j \binom{\gamma}{j} x((k-j)T_s) \quad (13)$$

Let's assume that the vector of continuous model derivation  $\gamma = [\gamma_1 \quad \gamma_2 \quad \cdots \quad \gamma_r]^T$ ,  $T_s$  is the sampling time and  $p \in \mathbb{N}$  is the number of past samples with which the derivation was computed.

If  $(i = 1, \dots, r)$ , the term  $\binom{\gamma}{j}$  can be written as follows:

$$\binom{\gamma}{j}^T = \left[ \binom{\gamma_1}{j} \quad \binom{\gamma_2}{j} \quad \cdots \quad \binom{\gamma_r}{j} \right] \quad (14)$$

$$\binom{\gamma_i}{j} = \begin{cases} 1 & \text{for } j = 0 \\ \frac{\gamma_i(\gamma_i - 1) \cdots (\gamma_i - j + 1)}{j!} & \text{for } j > 0 \end{cases} \quad (15)$$

By multiplying (13) by  $T_s^\gamma$  and developing the terms of  $j = 0$  and  $j = 1$  the following result is found:

$$T_s^\gamma D^\gamma x(t) = x(kT_s) - \gamma x((k-1)T_s) + \sum_{j=2}^p (-1)^j \binom{\gamma}{j} x((k-j)T_s) \quad (16)$$

Now let consider the following continuous fractional state-space model [12]:

$$\begin{cases} D^\gamma x(t) = A_c x(t) + B_c u(t) \\ y(t) = C_c x(t) \end{cases} \quad (17)$$

With  $A_c \in \mathbb{R}^{r \times r}$ ,  $B_c \in \mathbb{R}^{r \times 1}$  and  $C_c \in \mathbb{R}^{1 \times r}$  are the state matrices of the continuous fractional model and  $r$  is the number of variables in state-space model.

$$T_s^\gamma A_c x(kT_s) - x(kT_s) = -\gamma x((k-1)T_s) + \sum_{j=2}^p (-1)^j \binom{\gamma}{j} x((k-j)T_s) - B_c T_s u(kT_s) \quad (18)$$

Note that  $I_r \in \mathbb{R}^{r \times r}$  the identity matrix and  $T_s^\gamma$  the diagonal matrix filled by  $(T_s^{\gamma_1} \dots T_s^{\gamma_r})$ .

To facilitate writing, note

$$\mathbb{Z} = (T_s^\gamma A_c - I_r)^{-1} \quad (19)$$

$$x(kT_s) = -\mathbb{Z} \gamma x((k-1)T_s) + \mathbb{Z} \sum_{j=2}^p (-1)^j \binom{\gamma}{j} x((k-j)T_s) - \mathbb{Z} B_c T_s^\gamma u(kT_s) \quad (20)$$

and with  $(i = 1, \dots, r)$

$$c_j = \text{diag}\{(-1)^j \binom{\gamma_i}{j}\} \quad (21)$$

The above equation can be written as:

$$x(k) = \mathbb{Z} c_1 x(k-1) + \mathbb{Z} \sum_{j=2}^p c_j x(k-j) - \mathbb{Z} B_c T_s^\gamma u(k) \quad (22)$$

To simplify the equation:

$$A_j = \mathbb{Z} c_j \quad (23)$$

By expanding all terms and simplifying, (22) becomes in the form:

$$x(k) = A_1 x(k-1) + A_2 x(k-2) + \dots + A_k x(0) - \mathbb{Z} B_c T_s^\gamma u(k) \quad (24)$$

The system can therefore be described by a discrete state-space representation [13]:

$$\begin{cases} X_d(k+1) = A_d X_d(k) + B_d u(k) \\ y(k) = C_d X_d(k) \end{cases} \quad (25)$$

With

$$A_d = \begin{pmatrix} A_1 & A_2 & \dots & A_{p-1} \\ I & 0 & \dots & 0 \\ 0 & I & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & \dots & I & 0 \end{pmatrix}, \quad B_d = \begin{pmatrix} -\mathbb{Z} B_c T_s^\gamma \\ 0 \\ \vdots \\ 0 \end{pmatrix},$$

$$C_d = (C \quad 0 \quad \dots \quad 0)$$

$$X_d(k+1) = \begin{pmatrix} x(k+1) \\ x(k) \\ \vdots \\ x(k-p+1) \end{pmatrix} \quad \text{and}$$

$$X_d(k) = \begin{pmatrix} x(k) \\ x(k-1) \\ \vdots \\ x(k-p) \end{pmatrix}$$

with  $u$ ,  $y$ ,  $X_d$  are respectively the input, output and variables state of the process.  $p$  is the number of past iterations which the system takes into account for calculating a variable,  $A_d \in \mathbb{R}^{rp \times rp}$ ,  $B_d \in \mathbb{R}^{rp \times 1}$ ,  $C_d \in \mathbb{R}^{1 \times rp}$  and  $X_d \in \mathbb{R}^{rp \times 1}$ .

By increasing the number of iterations taken into account  $p$  the computation time increases, so it is reasonable to choose a number large enough to represent the system correctly but not too large to reduce the calculation time.

#### IV. FRACTIONAL MODEL PREDICTIVE CONTROL

The principle of the predictive control is to create an anticipatory effect for the system with respecting the trajectory to follow known in advance, based on the prediction of the future behavior of the system and minimizing the gap of these predictions to the trajectory and by minimizing a certain cost function  $J$ , while respecting operating constraints [14, 15, 16].

This section will develop a predictive control from the discrete fractional state-space model described in previous section. For that we will make a variable change:  $\Delta X_d(k) = X_d(k) - X_d(k-1)$  the input variable difference:  $\Delta u(k) = u(k) - u(k-1)$ , and using it in (25) this transformation is found:

$$\Delta X_d(k+1) = A_d \Delta X_d(k) + B_d \Delta u(k) \quad (26)$$

The new state variable vector is:

$$X(k) = [\Delta X_d(k)^T \quad y(k)]^T$$

with  $y(k)$  is the output and:

$$y(k+1) - y(k) = C_d A_d \Delta X_d(k) + C_d B_d \Delta u(k) \quad (27)$$

The system can be written in the form:

$$\begin{cases} X(k+1) = AX(k) + B\Delta u(k) \\ y(k) = CX(k) \end{cases} \quad (28)$$

$$A = \begin{pmatrix} A_d & 0_d^T \\ C_d A_d & 1 \end{pmatrix}; \quad B = \begin{pmatrix} B_d \\ C_d B_d \end{pmatrix};$$

$$C = (0_d \quad 1); 0_d \in \mathbb{R}^{1 \times rp}$$

Future state variables can be predicted and written in the form:

$$\begin{cases} X(k+1) &= AX(k) + B\Delta u(k) \\ X(k+2) &= AX(k+1) + B\Delta u(k+1) \\ &= A^2X(k) + AB\Delta u(k) + B\Delta u(k+1) \\ &\vdots \\ X(k+H_p) &= A^{H_p}X(k) + A^{H_p-1}B\Delta u(k) + \\ &A^{H_p-2}B\Delta u(k+1) + \dots \\ &+ A^{H_p-H_c}B\Delta u(k+H_c-1) \end{cases} \quad (29)$$

Based on (29) future system outputs can be predicted:

$$\begin{cases} y(k+1) &= CAX(k) + CB\Delta u(k) \\ y(k+2) &= CAX(k+1) + CB\Delta u(k+1) \\ &= CA^2X(k) + CAB\Delta u(k) + \\ &CB\Delta u(k+1) \\ &\vdots \\ y(k+H_p) &= CA^{H_p}X(k) + CA^{H_p-1}B\Delta u(k) + \\ &CA^{H_p-2}B\Delta u(k+1) + \dots \\ &+ CA^{H_p-H_c}B\Delta u(k+H_c-1) \end{cases} \quad (30)$$

$H_p$  and  $H_c$  are respectively the prediction horizon and the control horizon with  $H_p \geq H_c$ . Assume the vector  $Y$  which contains  $H_p$  system's predicted future outputs and  $\Delta u$  contains  $H_c$  future controls:

$$Y^T = [y(k+1) \ y(k+2) \ \dots \ y(k+H_p)]$$

$$\Delta u^T = [\Delta u(k) \ \Delta u(k+1) \ \dots \ \Delta u(k+H_c-1)]$$

The vector  $Y$  can also be written as :

$$Y = FX(k) + \Phi\Delta u \quad (31)$$

$$F = \begin{pmatrix} CA \\ CA^2 \\ CA^3 \\ \vdots \\ CA^{H_p} \end{pmatrix} \quad (32)$$

$$\Phi^T = \begin{pmatrix} CB & CAB & CA^2B & \dots & CA^{H_p-1}B \\ 0 & CB & CAB & \dots & CA^{H_p-2}B \\ 0 & 0 & CB & \dots & CA^{H_p-3}B \\ \vdots & \vdots & \vdots & \ddots & \vdots \\ 0 & 0 & 0 & & CA^{H_p-H_c}B \end{pmatrix} \quad (33)$$

The aim of predictive control is to find the control vector  $\Delta u$  which forces the system's output  $y$  to follow the setpoint

$y_s$ . In order to achieve this we must optimize a criterion  $J$  which represents the control objective:

$$J = \sum_{i=1}^{H_p} (y_s(k+i) - y(k+i))^2 + \lambda \sum_{i=0}^{H_c-1} \Delta u^2(k+i) \quad (34)$$

The criterion  $J$  can be written in matrix form:

$$J = (Y_s - Y)^T (Y_s - Y) + \Delta u^T \lambda \Delta u \quad (35)$$

With  $Y_s^T = [y_s(k+1) \ y_s(k+2) \ \dots \ y_s(k+H_p)]$  is the vector filled by the future values of the set-points and  $\lambda$  is weight coefficient on the control.

By minimizing  $J$  we obtain optimal control sequence [17]:

$$\Delta u = (\Phi^T \Phi + \lambda I)^{-1} \Phi^T (Y_s - FX(k)) \quad (36)$$

## V. SIMULATION RESULTS

In this section the matlab FOMCON toolbox is used to find a continuous fractional transfer function from the input-output data of a thermal system. The input signal used for identification is shown in the Fig.1. In this case we chose a free identification to find the better result.

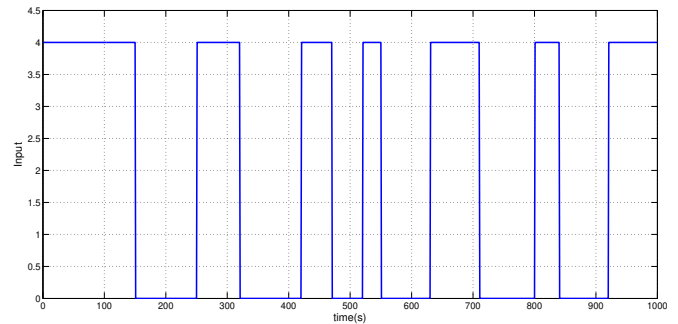


Fig. 1. System input.

The result obtained is compared with the output signal used in the identification, the Fig.2 illustrates the two signals as well as the error.

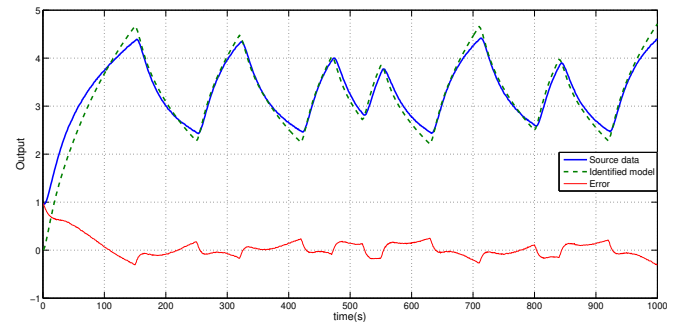


Fig. 2. Identification result.

This method gives as result a continuous fractional transfer function (7)

$$G(s) = \frac{b_0}{s^{2.46} + \tilde{a}_1 s^{1.97} + \tilde{a}_2 s^{1.39} + \tilde{a}_3 s^{0.97} + \tilde{a}_4 s^{0.88} + \tilde{a}_5} \quad (37)$$

So the parameters are deduced:  $b_0 = -0.0041$ ,  $\tilde{a}_1 = -1.5977$ ,  $\tilde{a}_2 = 0.551$ ,  $\tilde{a}_3 = -0.3517$ ,  $\tilde{a}_4 = -0.0011$  and  $\tilde{a}_5 = -0.002$ .

By applying the above method, the founded result is the fractional state-space representation for previous transfer function and which is described by the matrices:

$$A_c = \begin{pmatrix} 0 & 1 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 1 & 0 \\ 0 & 0 & 0 & 0 & 1 \\ 0.002 & 0.0011 & 0.3517 & -0.551 & 1.5977 \end{pmatrix},$$

$$B_c = \begin{pmatrix} 0 \\ 0 \\ 0 \\ 0 \\ 1 \end{pmatrix}, \quad C_c = (-0.0041 \quad 0 \quad 0 \quad 0 \quad 0)$$

$\tilde{\alpha}_1 = 0.88$ ,  $\tilde{\alpha}_2 = 0.97$ ,  $\tilde{\alpha}_3 = 1.39$ ,  $\tilde{\alpha}_4 = 1.97$  and  $\tilde{\alpha}_5 = 2.46$ .

and using (8) and (10) we can fill the vector  $\gamma$  by :

$$\gamma = \begin{pmatrix} \tilde{\alpha}_1 \\ \tilde{\alpha}_2 - \tilde{\alpha}_1 \\ \tilde{\alpha}_3 - \tilde{\alpha}_2 \\ \tilde{\alpha}_4 - \tilde{\alpha}_3 \\ \tilde{\alpha}_5 - \tilde{\alpha}_4 \end{pmatrix}, \quad \text{then} \quad \gamma = \begin{pmatrix} 0.88 \\ 0.09 \\ 0.42 \\ 0.58 \\ 0.49 \end{pmatrix}$$

From transfer function (37) the commensurate model that can be found by matlab FOMCON toolbox has a very high order, in this case  $r_c = 246$  and  $\alpha = 0.01$  With  $A_{c_c} \in \mathbb{R}^{r_c \times r_c}$ ,  $B_{c_c} \in \mathbb{R}^{r_c \times 1}$  and  $C_{c_c} \in \mathbb{R}^{1 \times r_c}$  are the state matrices of the continuous fractional model,  $\alpha$  is the commensurate order and  $r_c$  is the number of variables in state-space commensurate model.

For discretization the chosen sampling period is  $T_s = 5s$  and the history will be limited to 20 past values so  $p = 20$ , these parameters will be the same for the rest of this paper.

In what follows (Fractional Model Predictive Control) FMPC will be applied for both models, the necessary parameters for the FMPC will be fixed for this section  $H_p = 10$ ,  $H_c = 1$  and  $\lambda = 2$ .

The system output (temperature) and the set-point are shown in the Fig.3 while the Fig.4 shows the control signal generated by the FMPC. A disturbance is added to the system in the interval of time  $k \in [120, 150]$  to test the ability of FMPC to anticipate it, the amplitude of this disturbance is +10%.

Fig.3 compares the output of the non-commensurate model with the commensurate model, these two models are deduced from the same transfer function presented by (37).

The Fig.3 and Fig.4 show that the FMPC is able to mitigate the effect of the disturbance on the output. On the other hand the Fig.5 shows peaks with a very large amplitude which appears in the control increment signal.

The figures show that the predictive control is able to force the system to follow the set-point in both cases, but it is clear

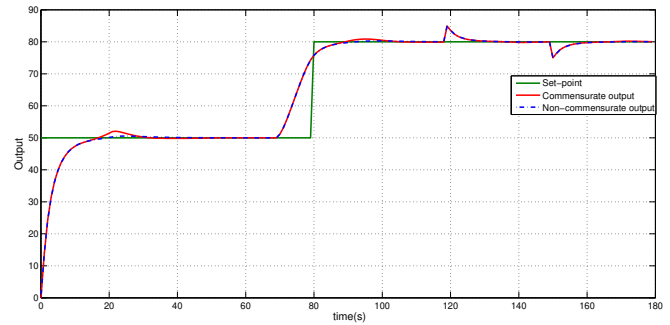


Fig. 3. Output with disturbance.

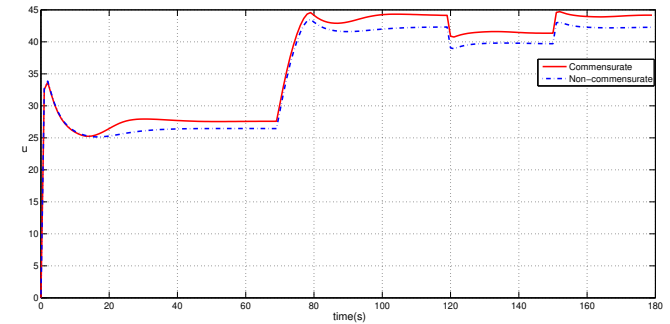


Fig. 4. Control with disturbance.

that for the non-commensurate model the control expends less energy to achieve it.

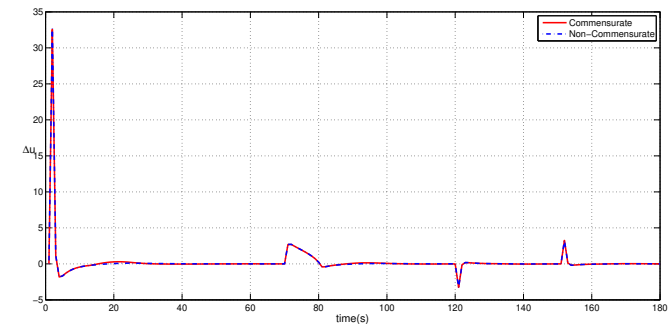


Fig. 5. Control increment with disturbance.

In the Fig.5, the control increases by a large amount instantly. To cancel this undesirable spike we will add a constraint to the calculation of control.

The principle of constraint control [18, 19] is to add to the main problem one or more conditions, it is therefore necessary to minimize criterion  $J$  while respecting these conditions. The most used constraint form is the one on the rate of change of the control variables  $\Delta u(k)$ . Suppose that for a single-input system the upper limit is  $\Delta u_{max}$  and the lower limit is  $\Delta u_{min}$ . The constraints are specified in the form:

$$\Delta u_{min} \leq \Delta u(k) \leq \Delta u_{max} \quad (38)$$

Assuming that the control variable  $\Delta u(k)$  can only increase or decrease in a unit of magnitude less than 2.5, the operational constraint is:

$$-2.5 \leq \Delta u(k) \leq 2.5$$

Now let's test the performance of the system under constraint and with a disturbance of amplitude +10% in the interval of time  $k \in [120, 150]$ , the constraint is the same used before.

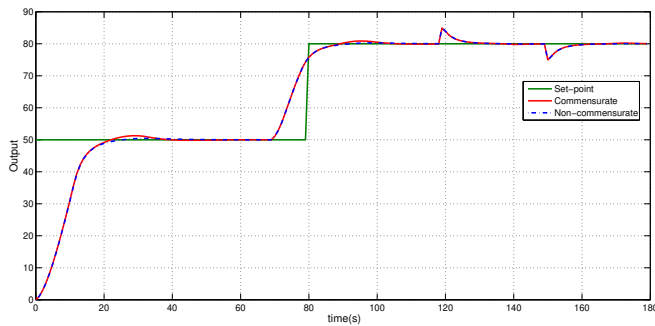


Fig. 6. Output with constraint and disturbance.

Even under constraint the FMPC can ensure that the output (temperature) follows the set-point. Constrains on the control increment guarantees that there is no peaks in the control signal. In return, the output pursuit becomes slower as shown in the Fig.6.

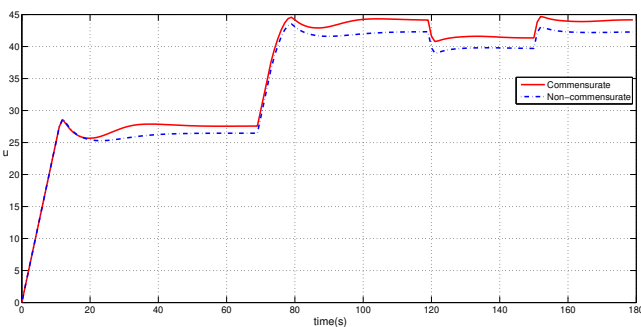


Fig. 7. Control with constraint and disturbance.

The choice of the the interval  $[\Delta u_{min}, \Delta u_{max}]$  is very important because if the interval is too wide the condition will not be taken into account when minimizing criterion  $J$ , and if the interval is too small the control will no longer be able to bring the output to follow the set-point, even if it happen the system will be too slow.

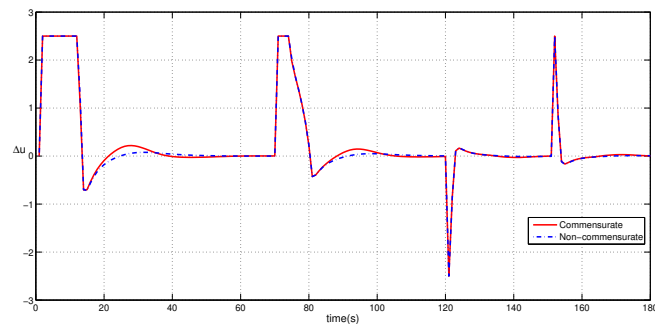


Fig. 8. Control increment with constraint and disturbance.

Fig.7 and Fig.8 show that the constraint is taken into account in optimisation and show that the non-commensurate model still expends less energy than the commensurate model.

One of the disadvantages of fractional systems is the increase of the dimensions of the matrices at each iteration. For

example if  $p = 20$ , the calculation of the state variables will depend on 20 previous values. The dimensions of the matrices will increase to multiply by  $p$ . This increase has a negative effect on the calculation time which increases considerably.

Now let's focus on the calculation time for both models. This part compares the time spent on each iteration to calculate the control increment  $\Delta u$  for different value of  $p$ . In this simulation the used processor is a  $i3$  with  $1.9 GHz$  frequency, the results are presented in Table I:

TABLE I. CALCULATE TIME (MS)

p	20	50	100	180
Non-commensurate	22.7	23.6	27.9	30.5
Commensurate	53.2	56.1	61.5	74.1

Even if fractional models better represent physical systems, their use can be complicated. The commensurate model has a very high order  $r_c = 246$  whereas in the case non-commensurate model  $r = 5$ , this difference is manifested in the computation time.

These results show that the use of the commensurate model can provide the same performance as non-commensurate model with a longer computing time. The non-commensurate model consecutively reduces the calculation time for the control because the matrices have a smaller dimension. On the other hand, the determination of a non-commensurate model is more complicated than the commensurate model.

## VI. CONCLUSION

The use of fractional models becomes more and more frequent given the efficiency they provide in the discription of certain physical systems. Nevertheless it remains a little difficult to handle. The majority of research [20, 21, 22] deals with commensurate fractional models that have proved efficiency at describing several physical phenomena, but the major inconvenience is that computation time increases in discrete models because of the use of history in the calculation. This article has shown that the limitation of the used history and the use of non-commensurate models in modeling or identification can remedy this problem. It has also adapted predictive control to apply it to a non-commensurate fractional system. The importance of this work is that it deals with the state-space representation of the non-commensurate fractional systems from identification to control. It also compares the use of commensurate and non-commensurate fractional systems and explores the advantages and disadvantages of each model. At first it introduced the transition between the transfer-function and the state-space representation in the non-commensurate fractional case. Then for the same kind of system, it explained the discretization and we closed by a comparison with the commensurate model in term of performance and computation time.

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